



EMERSON EXCHANGE 2025

ACCELERATING INNOVATION



ACCELERATING
INNOVATION

Sizzling Control: How implementing a MPC Upgrade Delivered Big Wins

Session ID: 3-1258

Disclaimer

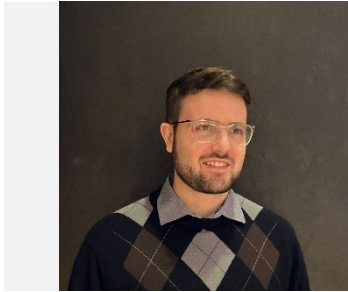
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Lou Heavner

Viscofan Overview

Context

Problem Statement

Proposed Solution

Execution

Results

Conclusion



Viscofan– Global Leader in Casing Solutions

Viscofan is the **world's leading producer and distributor of artificial casings for the meat industry.**

- Leads the industry as the only company with all major casing technologies (cellulose, collagen, fibrous and plastic).
- Ensures global reach with 20 manufacturing sites, 15 of which produce casings, across 12 countries.
- Serves a diverse customer base by expanding its commercial network to more than 100 countries.

OUR SITE



Danville Site

- This is the largest Viscofan facility in the United States for which it plays a pivotal role in the organization.
- Its origins trace back to 1957, when it was built by Teepak.
- The site was acquired by Viscofan in 2006.
- Specializes in cellulose casings, primarily used for hot dogs and frankfurters, designed for easy peeling after cooking.
- Produces fibrous casings, essential for larger processed meats like salami and deli hams, offering strength and controlled expansion.
- Alongside production and manufacturing systems, Viscofan inherited OT/IT technologies for process control.



Context: Digital Transformation in an older plant

Brief History

- Since 1957, the factory has undergone several transformations
- It was owned by multiple corporations before Viscofan acquired it in 2006.
- With the different stakeholders, machines, processes and knowledge has suffered radical changes.
- Control systems were no exception; before the implementation of DeltaV the factory relied on a PIMS computer program from Biles & Associates named AIM. It was originally connected to PROVOX, a legacy Emerson product.

Legacy Control

- AIM was critical for the plant as it helped automate process control in different production areas.
- The previous generation of control included the PROVOX DCS connected to the Biles & Assoc. AIM PIMS system. Both are obsolete.
- AIM controls could be categorized as expert systems, that highly specialized chemical and process engineers used to program and maintain.
- However, due to the many transformations the factory underwent, a lot of knowledge was lost.

Contemporaneous Control

- DeltaV was implemented in Danville, 18 years ago and Viscofan has migrated most of the legacy controls.
- DeltaV is the main DCS in the plant.
- Alongside it, other systems, such as AVEVA PI were implemented.
 - The obsolete Biles & Assoc AIM package remained, providing crucial control functionality
 - The sole support engineer retired
- The advanced process control capabilities available within the DeltaV system, enabled Viscofan to migrate 100% from AIM.

Context: The Skinless Curing Process

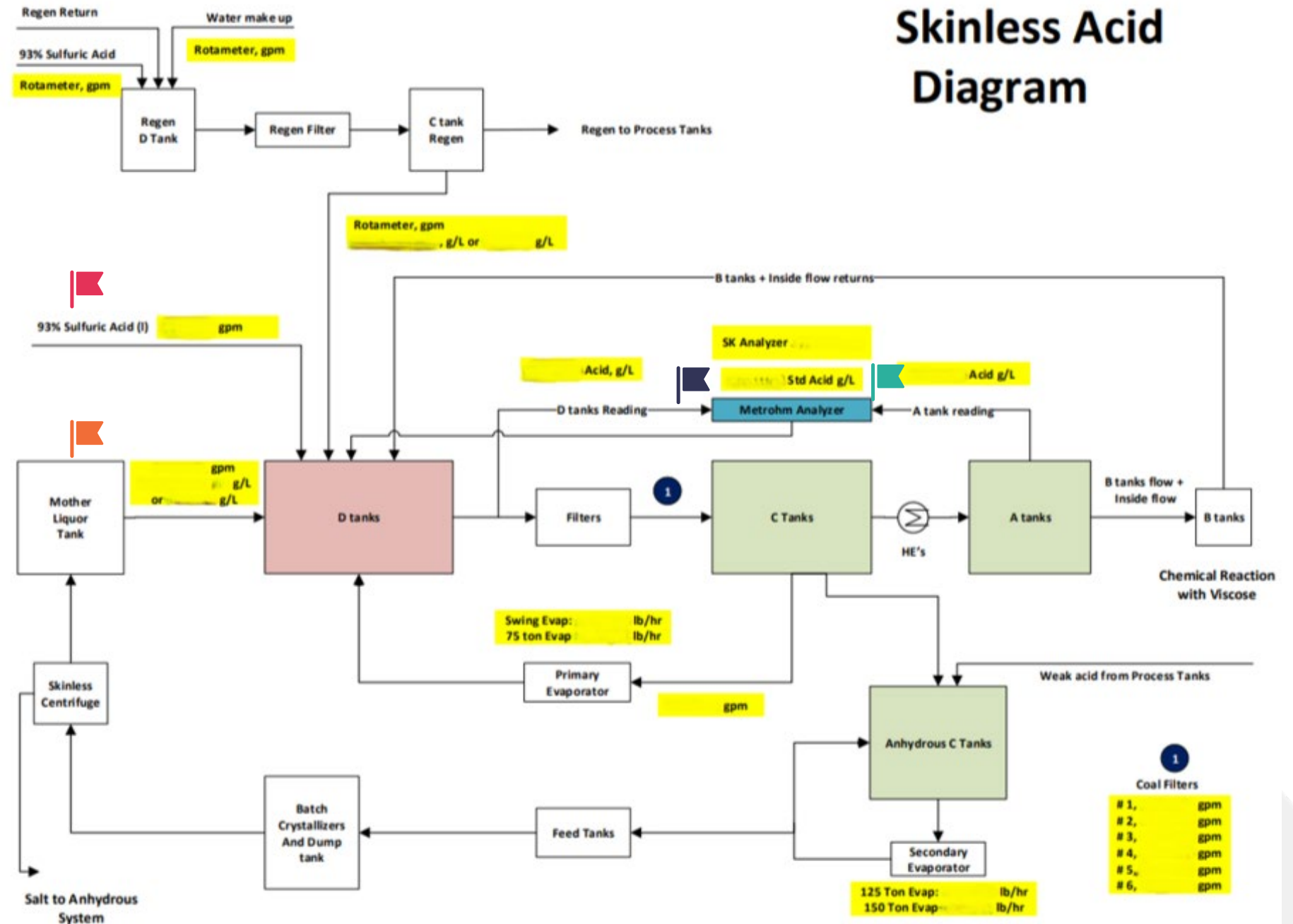
Skinless Acid Diagram

1 MV: Acid Flow

1 DV: Mother Liquor Flow

1 CV: Acid Concentration in A tank

1 LV: Acid Concentration in D tank



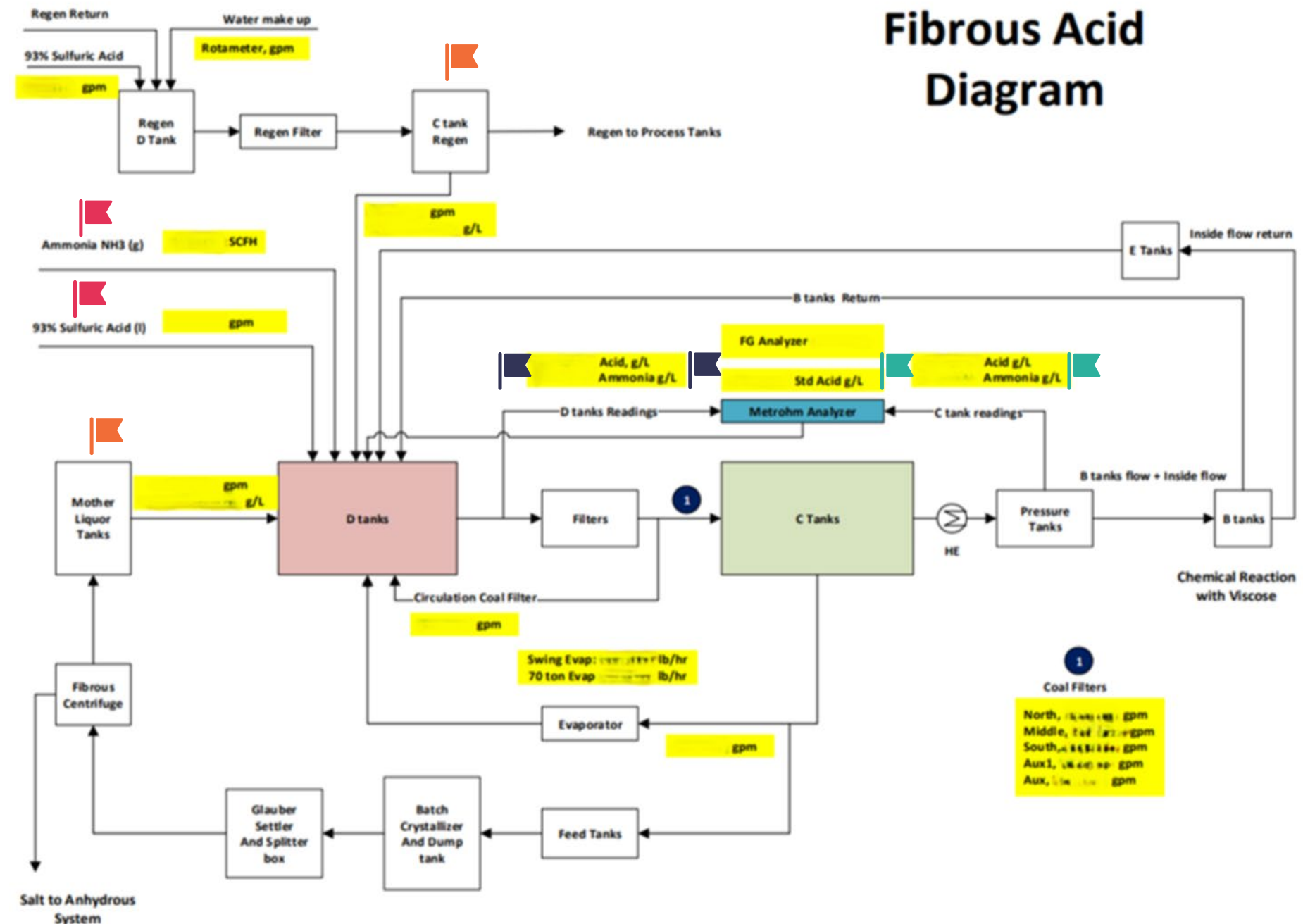
Context: The Fibrous Curing Process

2 MV: Acid & Ammonia Flows

2 DV: Mother Liquor & Regen Flows

2 CV: Acid & Ammonium Sulfate Concentrations in A tank

2 LV: Acid & Ammonium Sulfate Concentrations in D tank



Context: AIM System Usability

```
AIM.rdox
AIM VERSION NO. 7.4-1          14-MAR-2025 12:42:35
TEEPAK, LLC                    AIM Extended Console System      Size Code "R"

AIMecs AIMENU

A ALARM SUMMARY DISPLAY
D STATISTICAL PROCESS CONTROL
F AIM DBIF INTERACTIVE REQUEST
I DIGITAL INPUT DISPLAY
K CLIENT DEFINED USER MENU
N INACTIVE VARIABLE SUMMARY
P PROCESS VARIABLE DISPLAY
S SETUP MENU
U AIM UTILITIES MENU
W TUNING PARAMETER DISPLAY
Z REAL-TIME SPC DISPLAY
ECS MENU HELP
@CUSTDAT:CUSTOMER HELP

C OFF COMPUTER CONTROL SUMMARY
E HISTORIAN TABULAR DATA DISPLAY
H HISTORIAN DATA DISPLAY
J HISTORIAN TEXT VARIABLE DISPLAY
M MISCELLANEOUS VARIABLE DISPLAY
O DIGITAL OUTPUT DISPLAY
R ALARM HISTORY DISPLAY
T TEXT VARIABLE DISPLAY
V PROCESS GRAPHIC DISPLAYS
Y AIMTRAK SELECTION
Q QUIT EXTENDED CONSOLE SYSTEM
@AIMROOT:AIM HELP

Welcome To Biles & Associates AIM
For a description of the new features in this release, position the cursor to
@AIMROOT:AIM_HELP and press the HELP key. Then select AIM_RELEASE.
Ask for help on the sub-topics that are items of interest for you.
```

Context: AIM System Usability

AIM.rdox

AIM CALCULATION GENERATOR

page 1

1 - BLENDFLOW	17 - FIBML_CAL	33 - GW_CLEAR
2 - CAUSTIC50_TOT	18 - FIBML_SMOOTH	34 - HPS_TOTAL_FLOW
3 - COAGADAPT	19 - FIBPPR_UPD	35 - INI_ACID_EVENTS
4 - COAGCPID	20 - FIBREGADI	36 - MODE_PCT
5 - COAGDSET	21 - FIB_BTEMP_AVG	37 - OPC_POINTS
6 - COAGLIMIT	22 - FIB_COAGD	38 - PAV_BSCHED_MON
7 - COAGML01	23 - FIB_CPID	39 - QCLAB_W_STD_TIME
8 - COAGMONI	24 - FIB_EVAP_TEMP	40 - REFRESHER
9 - DLDRIPRES	25 - FIB_EV_PO	41 - SCRUBBER_CAUSTIC
10 - DRYER_SPEED	26 - FIB_EXCH	42 - SHIFTMARK
11 - FG_APPLIKON	27 - FIB_GRAVITY	43 - TRAIN_ALM
12 - FIBAPPLIC	28 - FIB_LEVL3	44 - TRENCH
13 - FIBAVG	29 - FIB_SODIUM_SALT	45 - VISCOSE_SM_DAILY
14 - FIBCOAG_MONI	30 - FIB_SR_FILT	46 - VISS8
15 - FIBC_COAG_FILT	31 - FIB_STDTIME	47 - VISSOLVER_BIAS
16 - FIBD_COAG_FILT	32 - FITBLNDFLOW	48 - WBLEND_DUP_TEMP

Context: AIM System Usability

- Over 20 pages of code in a script
- Multiple Scripts per control strategy
- No GUI
- No mouse
- Hard to keep versions
- Diffused documentation (Only printed copies and notebooks)
- Limited memory
- A lot of comments with unorganized dates and variables.

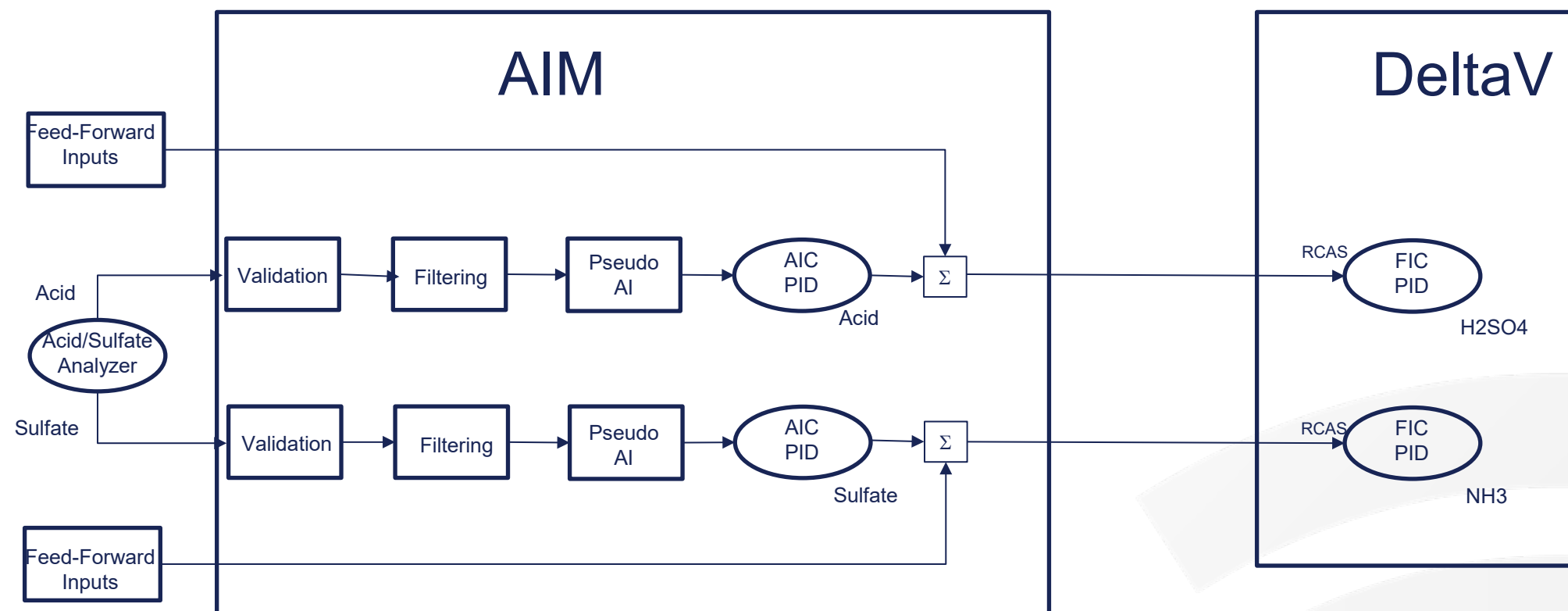
```

AIM.rdox
% Long before 12/22/2016: Adjust value of "wp_std_del", the devi
% target, if one value of wp_std_del has high absolute value. I
% adjust the filtered values based on the previous standard devi
% target, when the previous value is within +/-0.882 (3 sigma lim
% If both the current and previous value are outside of 3 sigma
% this is considered validation of the extreme deviation, and th
% deviation is applied. (CJR 10/11/2000)
    holdstd=laststd !for troubleshooting purposes only, in adump
if(abs("wp_std_del$amvcur")>0.882)then !a
    t1=abs(laststd-"ac10-628s$apvtar")
if(t1<0.882)then !b
    std_del=laststd-"ac10-628s$apvtar" !only 1 bad standard
else !b
    teststd=laststd-"ac10-628s$apvtar"
if((teststd<0.and."wp_std_del$amvcur"<0)
#.or.(teststd>0.and."wp_std_del$amvcur">0))then !c
    std_del="wp_std_del$amvcur" !2 or more standards outside 3 si
endif !c
endif !b
else !a
    std_del="wp_std_del$amvcur" !normal standards, withing 3 sig
  
```

Problem Statement

- Replacement of obsolete optimization package
 - Must be Integrated with DeltaV
 - User Interface requirements
 - Must be Integrated with online sampling analyzers
 - Asynchronous Inputs
 - Input Validation Required
 - Must be Easy for non-programmer
 - Supported by plant staff
 - Viscofan to self-perform project with limited Emerson consultation
 - Must faithfully reproduce AIM functionality
 - Closed Loop Supervisory Control
 - Analyzer validation & filtering
- Scope
 - Skinless Line curing (1 MV – acid flow)
 - Fibrous Line curing (2 MVs – acid flow & ammonia flow)

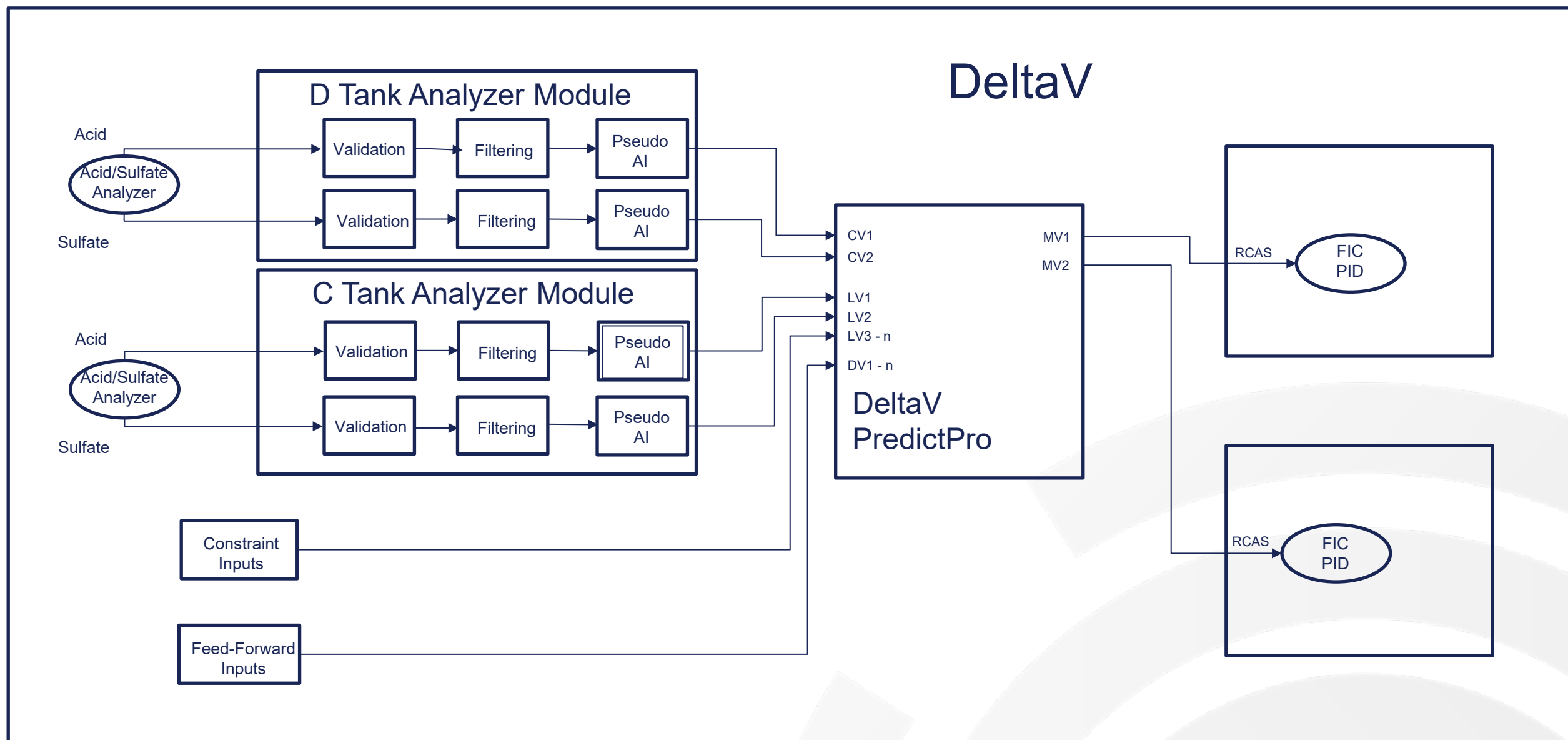
Original Control Structure



Proposed Solution

- DeltaV PredictPro replaces the AIM Control functionality
 - MPCPlus Block
 - Embedded in DeltaV
 - Ideal for slow deadtime dominant process
 - No license required for 1 MV configuration (prototype/proof of concept)
- Analyzer Input Block and Module replaces AIM analyzer validation functionality
 - Embedded in DeltaV (Composite Block)
 - Performs Validation Checks (Bad Input, Calibration, etc.)
 - Designed to work with PredictPro
- Design
 - Skinless - 1 MV, 1 CV, 1 LV, 2 DVs
 - Fibrous - 2 MV, 2 CV, 2 LV, 2 DVs

Proposed Structure



Project Execution

- Define Scope
- Decode AIM package
- Design
- Configure & Test
- Step Test
- Model Identification and Verification
- Commissioning
- Continuous Improvement

Decoding AIM package

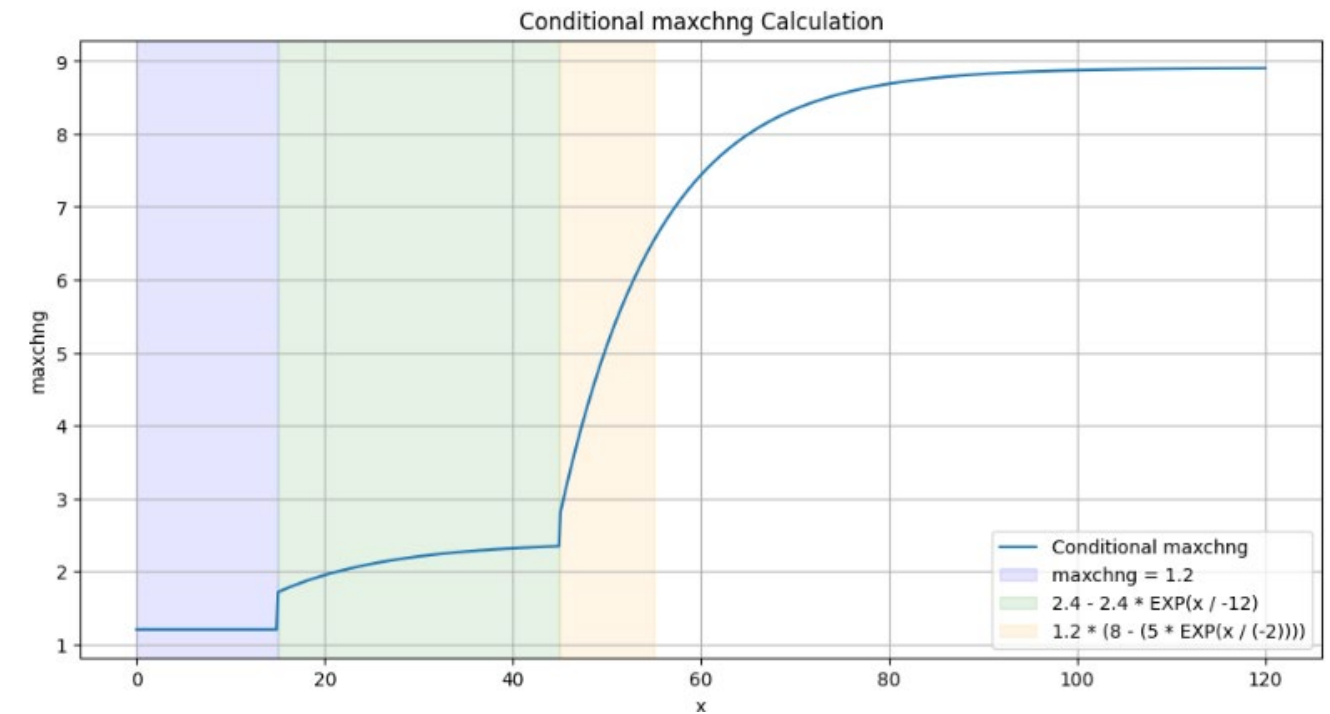
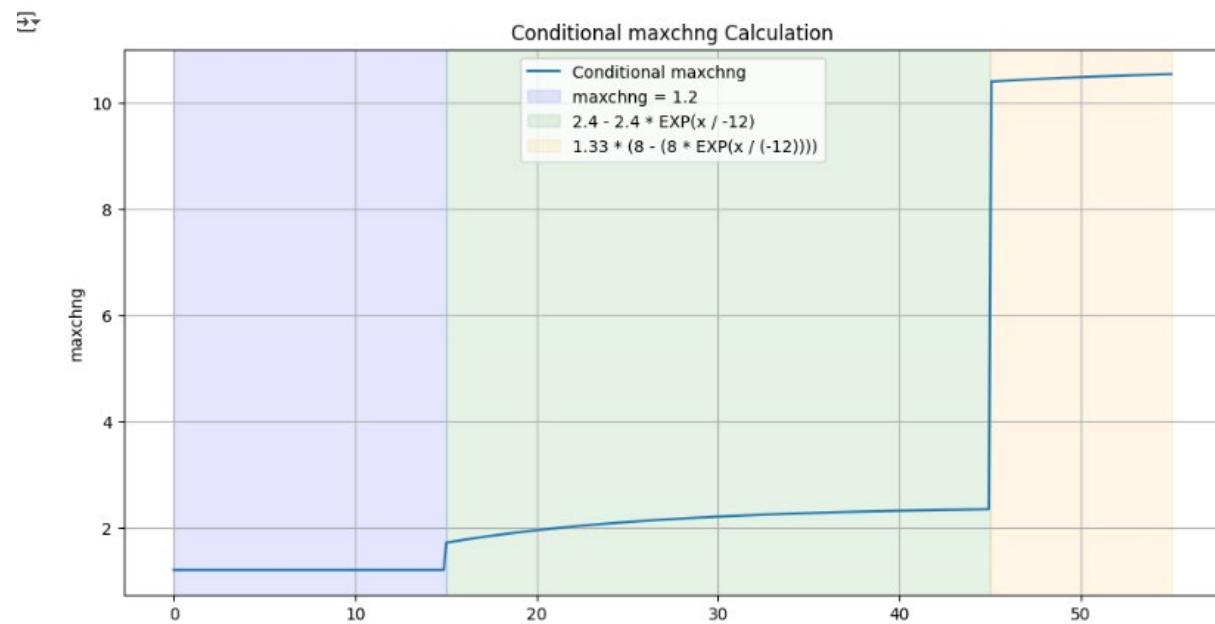
```

AIM.rdox
% Long before 12/22/2016: Adjust value of "wp_std_del", the deviation of the st
% target, if one value of wp_std_del has high absolute value. In that case,
% adjust the filtered values based on the previous standard deviation from
% target, when the previous value is within +/-0.882 (3 sigma limits).
% If both the current and previous value are outside of 3 sigma limits,
% this is considered validation of the extreme deviation, and the current
% deviation is applied. (CJR 10/11/2000)
  holdstd=laststd !for troubleshooting purposes only, in adump or test
if(abs("wp_std_del$amvcur")>0.882)then !a
  t1=abs(laststd-"ac10-628s$apvtar")
if(t1<0.882)then !b
  std_del=laststd-"ac10-628s$apvtar" !only 1 bad standard
else !b
  teststd=laststd-"ac10-628s$apvtar"
if((teststd<0.and."wp_std_del$amvcur"<0)
#.or.(teststd>0.and."wp_std_del$amvcur">0))then !c
  std_del="wp_std_del$amvcur" !2 or more standards outside 3 sigma
endif !c
endif !b
else !a
  std_del="wp_std_del$amvcur" !normal standards, withing 3 sigma

```

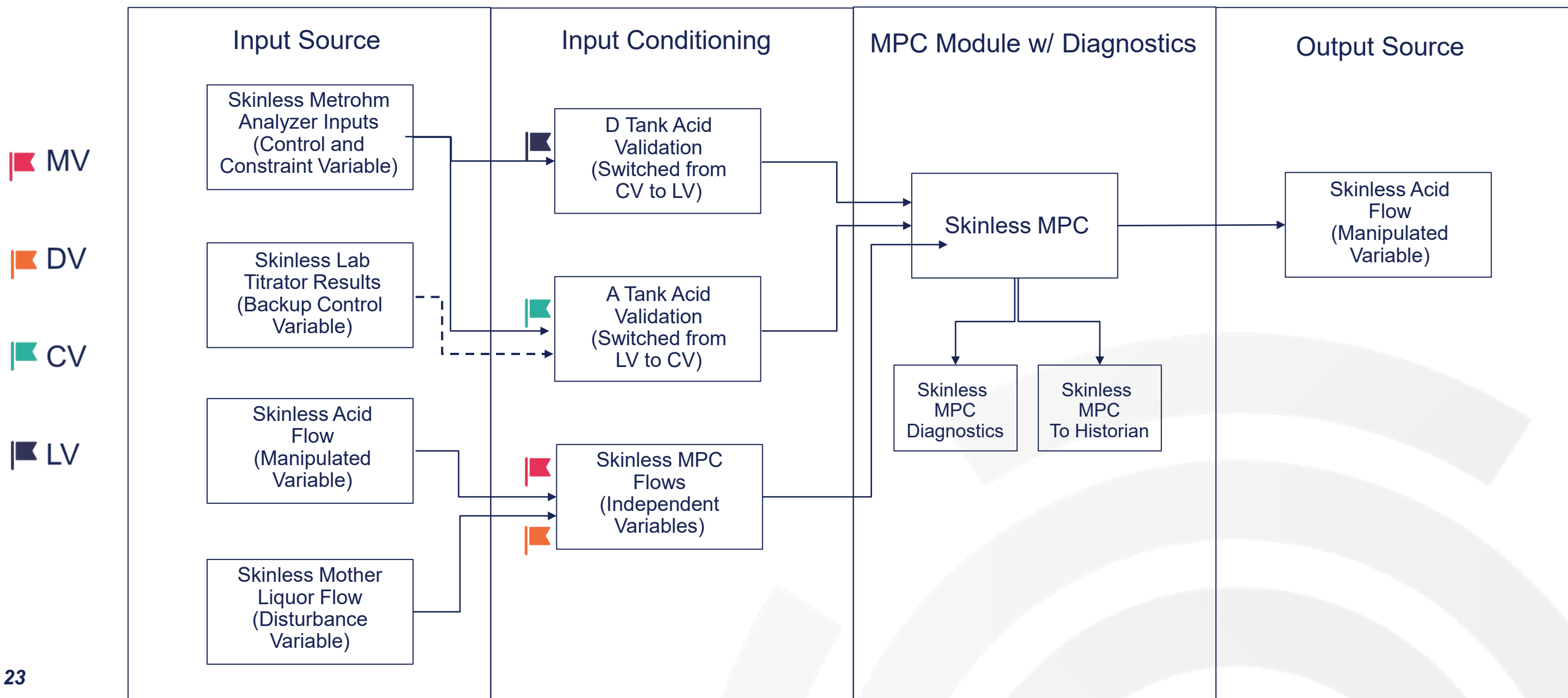

Analyzer Conditioning Requirement

- Minimum change to be new result
- Maximum change to be a valid result
 - Maximum change limit is dependent on time since last result.
 - AIM used step limits. DeltaV used filtered limits.



Design

Skinless



Design

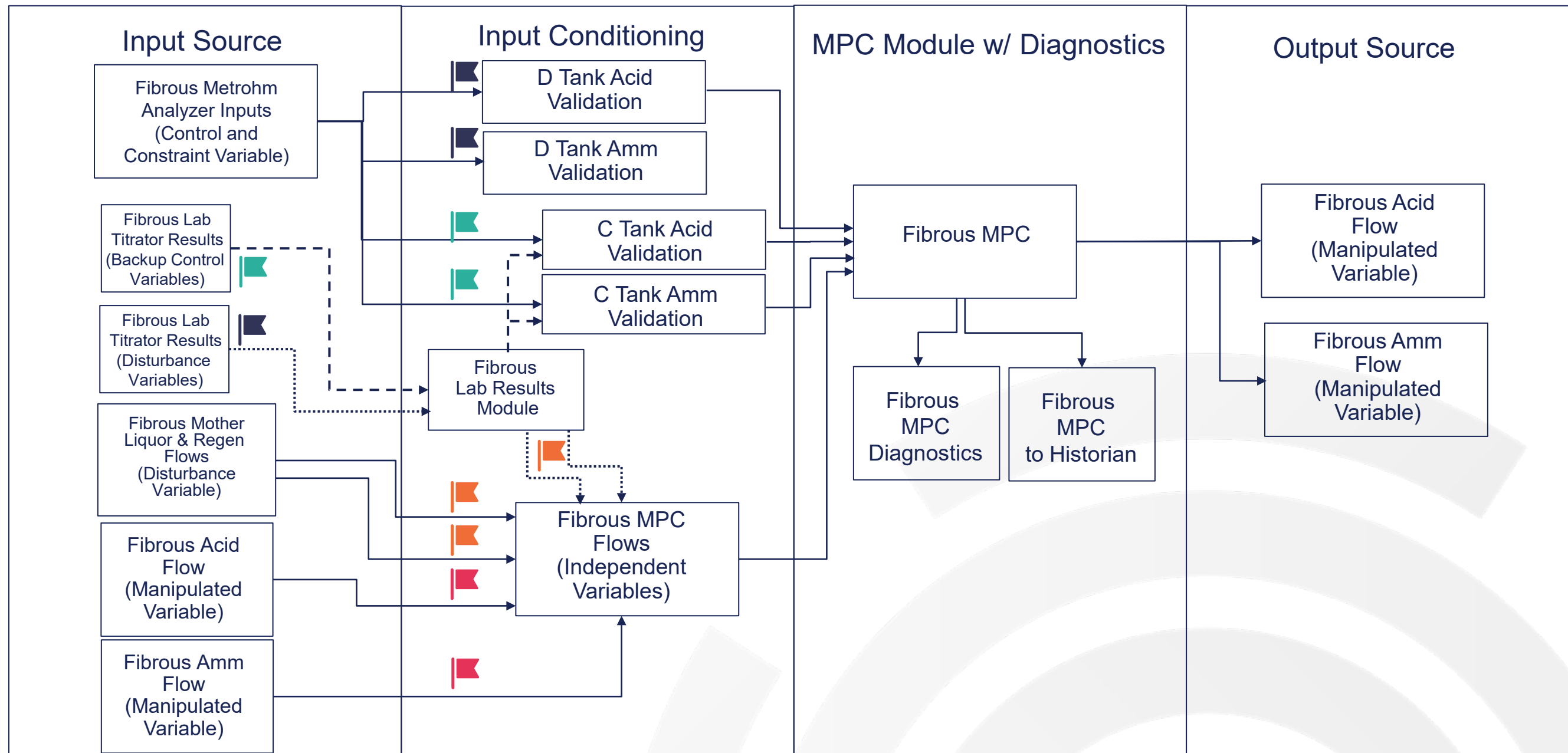
Fibrous

MV

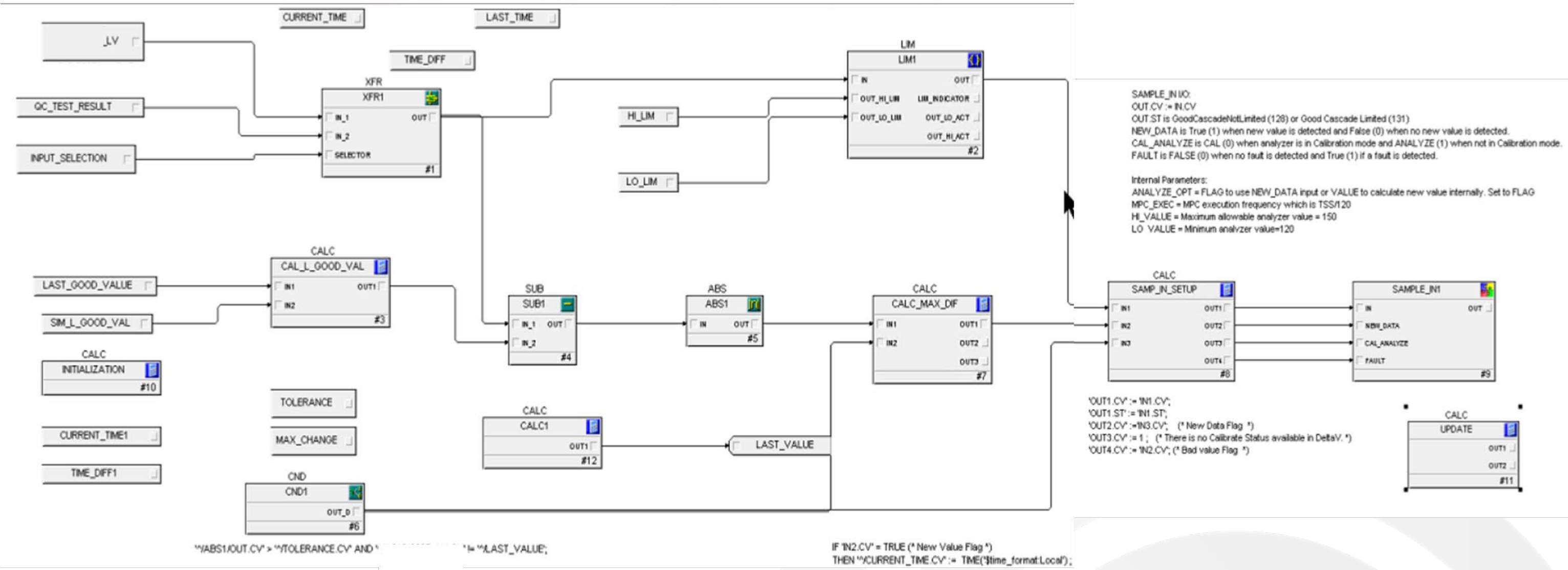
DV

CV

LV



Analyzer Input Configuration



PredictPro Configuration

MPC-PLUS1 Properties

Description	Track SP	Respon...	SP Low...	SP High...	Path
	Yes	0	125	135	UT

Total number of process inputs: 2 Total number of process outputs: 2 History sample rate: 1 sec

MPC-PLUS1 Properties

Description	Low Limit	High Limit	Maximu...	Path
	0	5	0.00016	

Total number of process inputs: 2 Total number of process outputs: 2 History sample rate: 1 sec

MPC-PLUS1 Properties

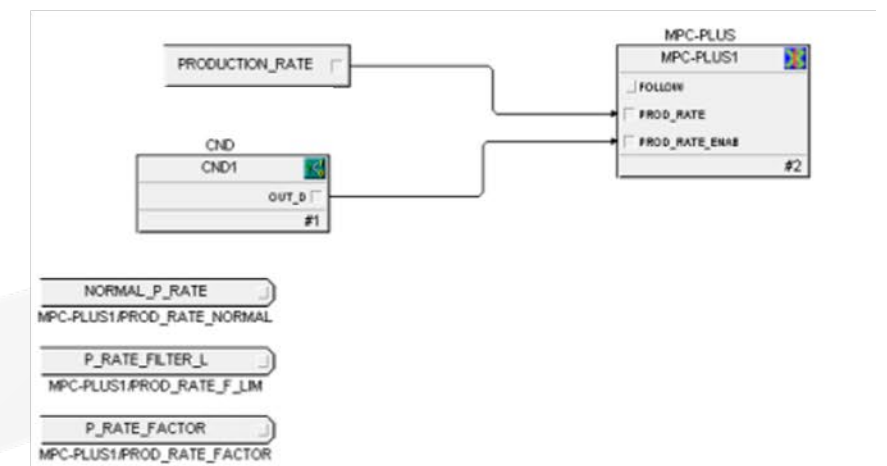
Description	Path
	JT

Total number of process inputs: 2 Total number of process outputs: 2 History sample rate: 1 sec

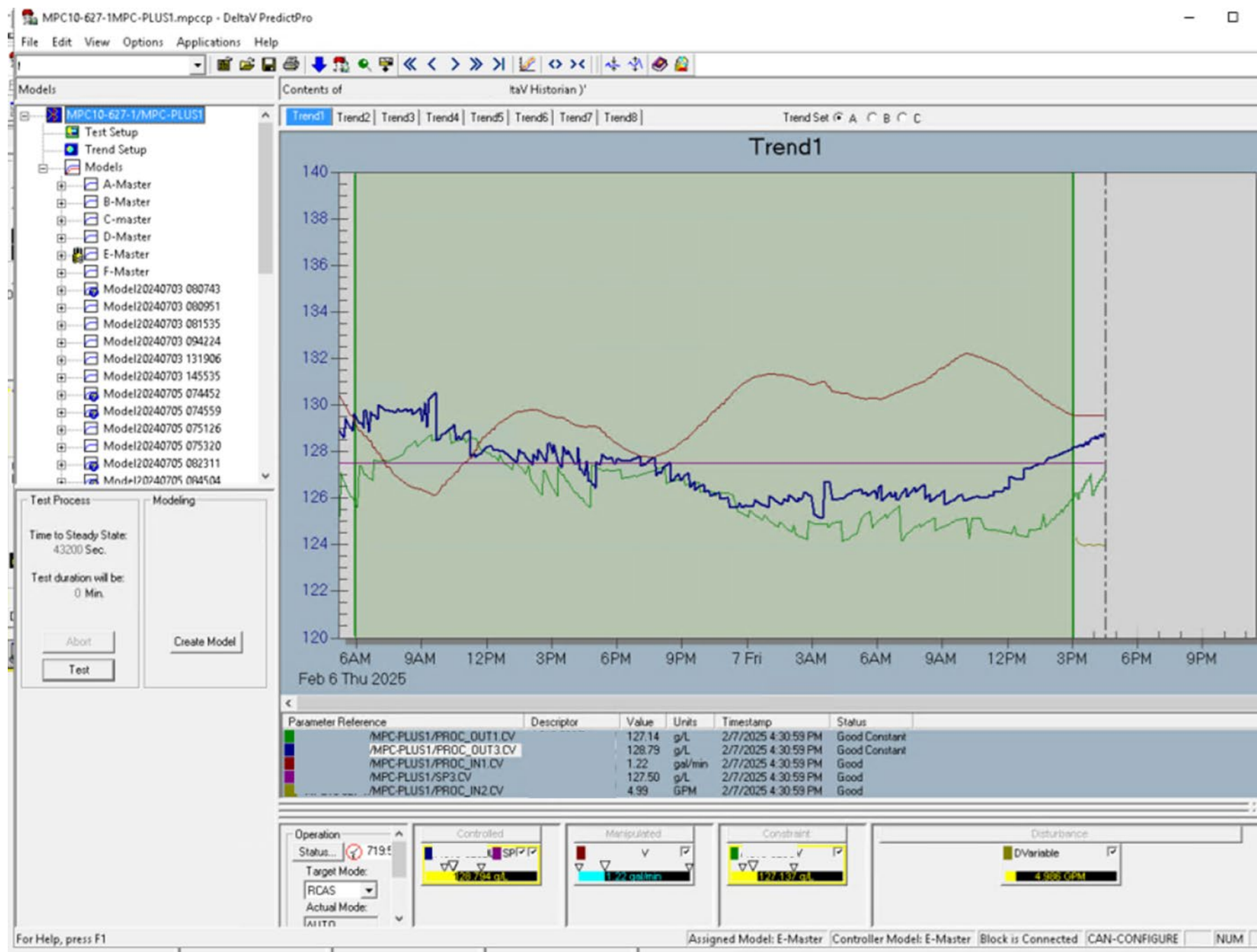
MPC-PLUS1 Properties

Description	Low Limit	High Limit	Path
J	123	137	IT

Total number of process inputs: 2 Total number of process outputs: 2 History sample rate: 1 sec



Model Identification



Model Identification

AutoSave Off 20240805 specifications Coag Acid Control.xlsx No Label • Saved to this PC

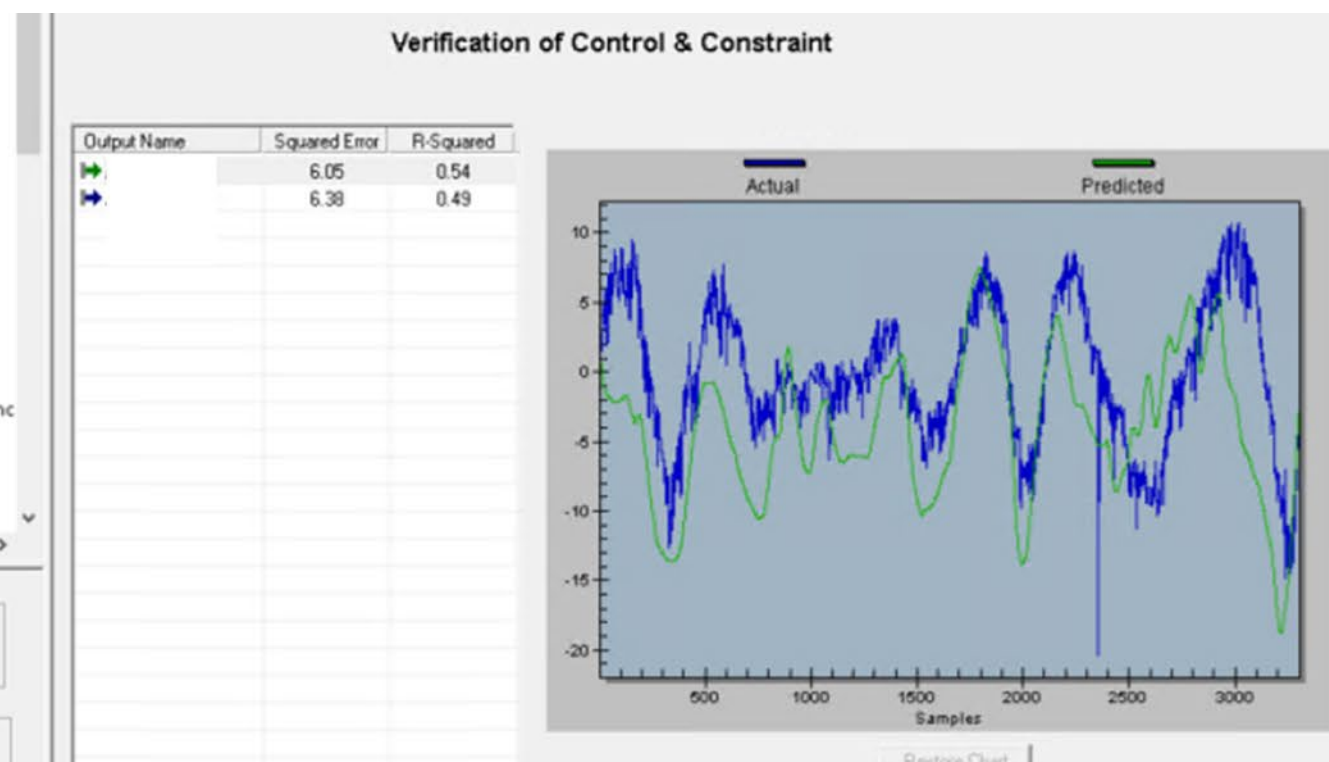
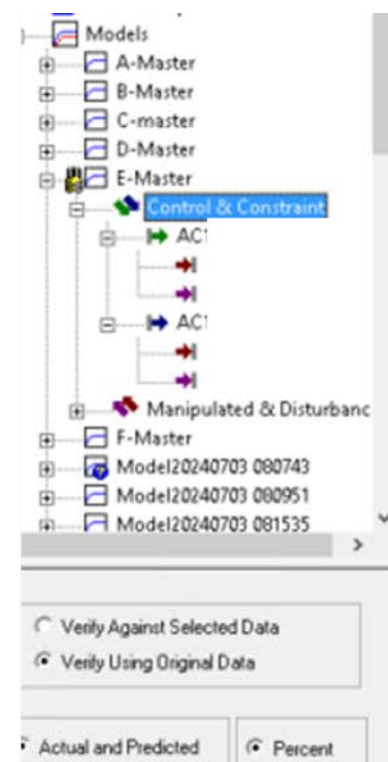
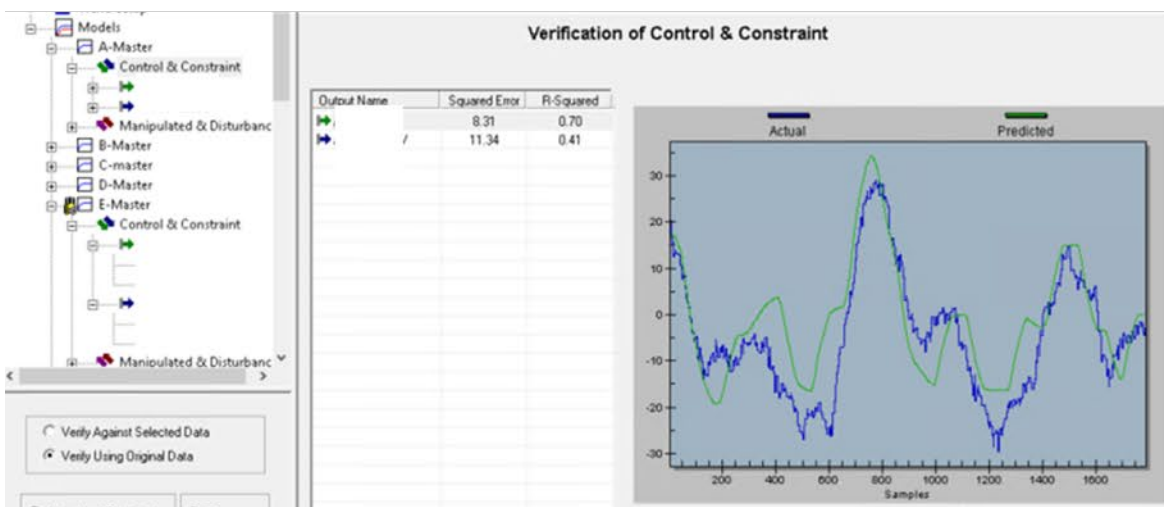
File Home Insert Draw Page Layout Formulas Data Review View Automate Developer Help Acrobat PI DataLink PI Builder Power Pivot

Clipboard Font Alignment Number Styles Cells Editing Analysis Sensitivity

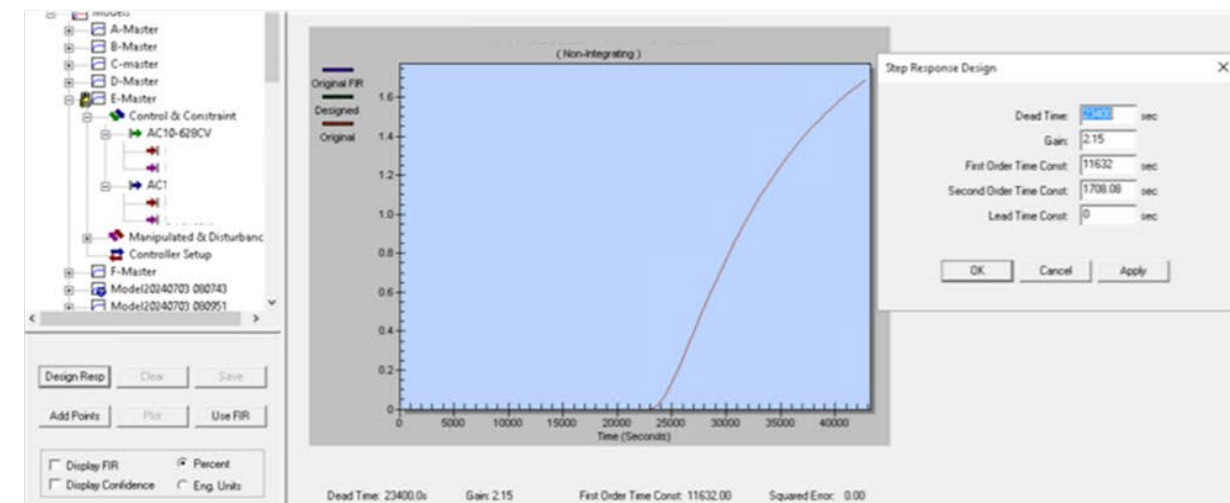
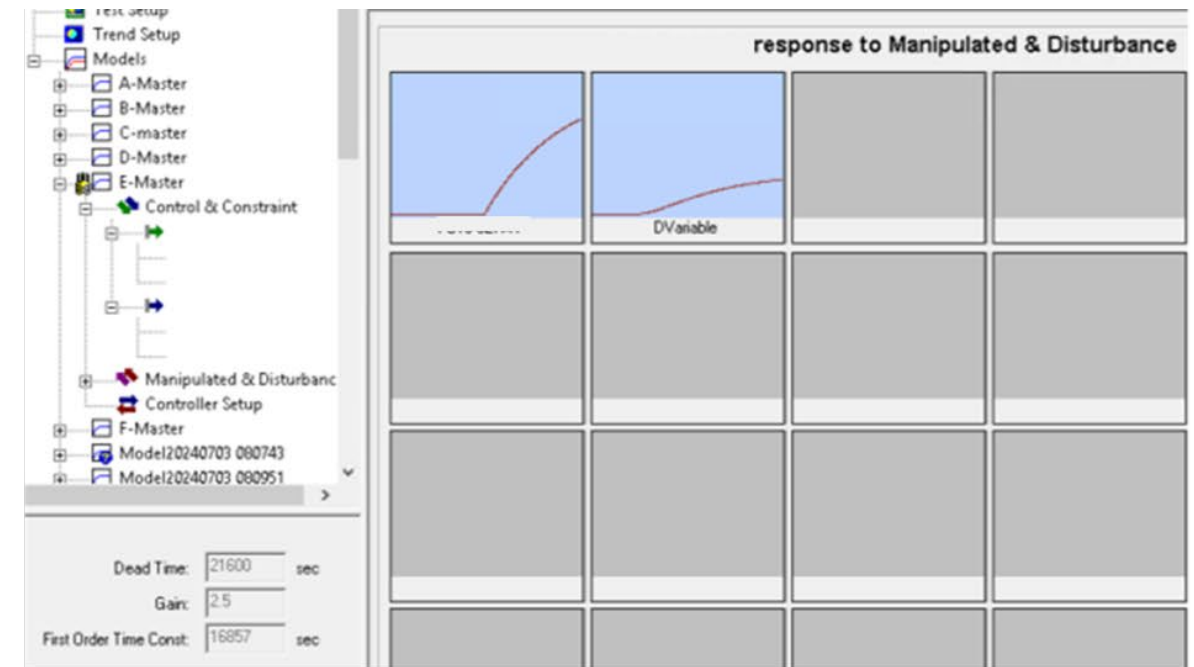
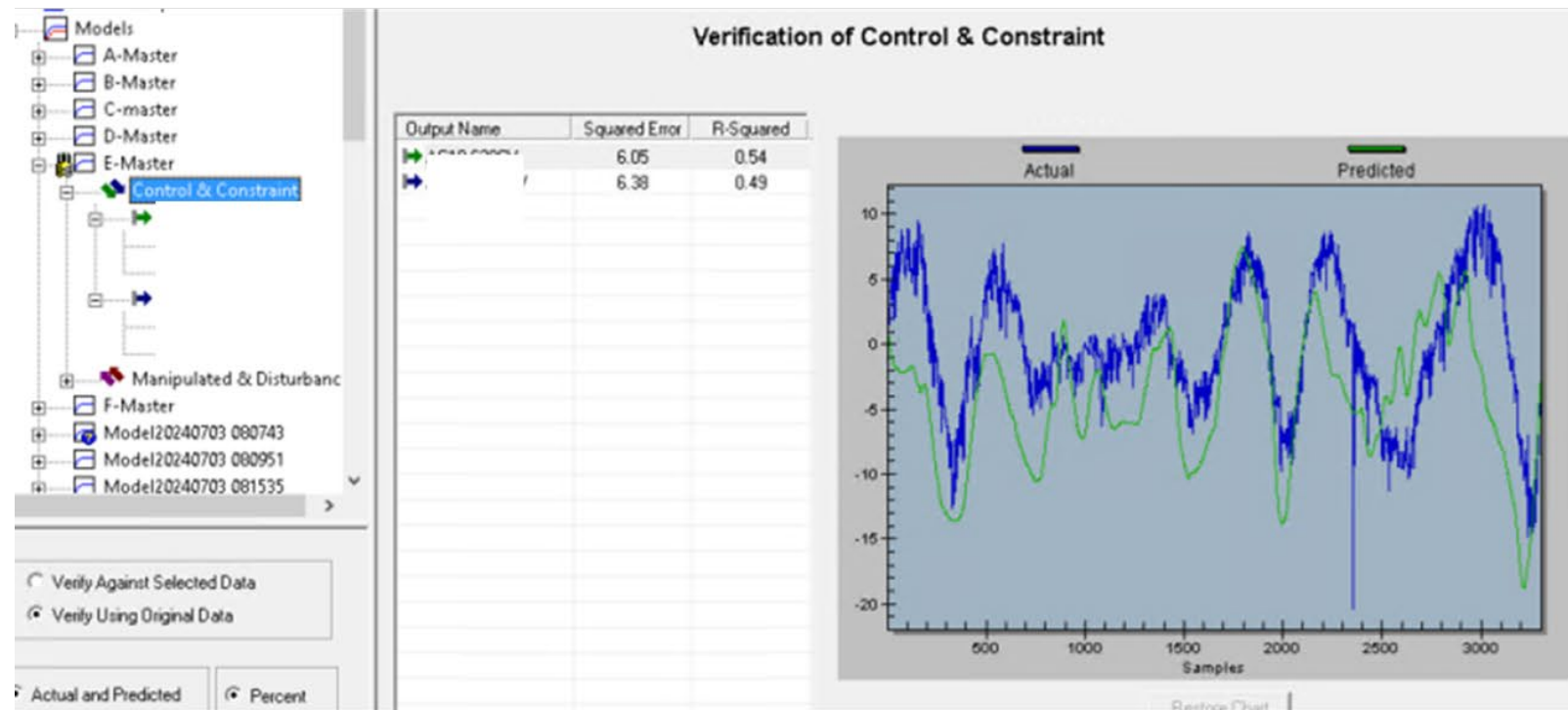
H11

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q
1	Date	V Type	Model	Error	R Squared		V Type	Model	Mean Error	Mean R Squared	Max Error	Min Error	Max RSq	Min RSq	Estimated StdDev Error	Estimated StdDev RSq	
2	7/30/2024	Control Variable	A	6.35	0.51		Control Variable	A	5.03	0.56	6.35	4.29	0.62	0.51	0.515	0.0275	
3	7/30/2024	Control Variable	C	6.92	0.47		Limit Variable	A	5.18	0.27	5.59	4.65	0.33	0.23	0.235	0.025	
4	7/30/2024	Control Variable	D	6.02	0.52		Control Variable	C	5.36	0.53	6.92	4.52	0.59	0.47	0.6	0.03	
5	7/30/2024	Control Variable	E	5.07	0.51		Limit Variable	C	5.27	0.29	5.68	5.04	0.35	0.26	0.16	0.0225	
6	7/30/2024	Limit Variable	A	4.65	0.33		Control Variable	D	5.08	0.56	6.02	4.35	0.59	0.52	0.4175	0.0175	
7	7/30/2024	Limit Variable	C	5.05	0.35		Limit Variable	D	5.22	0.40	5.56	5.02	0.46	0.37	0.135	0.0225	
8	7/30/2024	Limit Variable	D	5.21	0.46		Control Variable	E	4.81	0.53	5.82	3.98	0.55	0.51	0.46	0.01	
9	7/30/2024	Limit Variable	E	4.75	0.44		Limit Variable	E	5.05	0.36	5.42	4.75	0.44	0.32	0.1675	0.03	
10	7/31/2024	Control Variable	A	4.92	0.56		Control Variable	F	4.99	0.55	5.51	4.26	0.56	0.54	0.3125	0.005	
11	7/31/2024	Control Variable	C	5.39	0.52		Limit Variable	F	5.19	0.39	5.53	4.99	0.4	0.37	0.135	0.0075	
12	7/31/2024	Control Variable	D	4.74	0.57												
13	7/31/2024	Control Variable	E	4.21	0.55												
14	7/31/2024	Limit Variable	A	5.13	0.24												
15	7/31/2024	Limit Variable	C	5.33	0.27												
16	7/31/2024	Limit Variable	D	5.26	0.38												
17	7/31/2024	Limit Variable	E	5.03	0.34		=20*180										
18	8/1/2024	Control Variable	A	5.41	0.57		3600										
19	8/1/2024	Control Variable	C	5.62	0.55												
20	8/1/2024	Control Variable	D	5.51	0.57												
21	8/1/2024	Control Variable	E	5.33	0.53		StDev = (Maximum - Minimum)/4										
22	8/1/2024	Control Variable	F	5.51	0.55												
23	8/1/2024	Limit Variable	A	5.59	0.27												
24	8/1/2024	Limit Variable	C	5.68	0.28												
25	8/1/2024	Limit Variable	D	5.56	0.39												
26	8/1/2024	Limit Variable	E	5.42	0.35		Start time	7/16/2024	10:00 AM								
27	8/1/2024	Limit Variable	F	5.53	0.39												
28	8/2/2024	Control Variable	A	4.29	0.62												
29	8/2/2024	Control Variable	C	4.52	0.59		V Type	Model	Mean Error	Mean R Squared	Max Error	Min Error	Max RSq	Min RSq	Estimated StdDev Error	Estimated StdDev RSq	
30	8/2/2024	Control Variable	D	4.99	0.59		Control Variable	A	AVERAGEIFS(D	AVERAGEIFS(E:E,E	MAXIFS(D:MINIFS(D:MAXIFS(E:MINIFS(E:(K30-L30)/4					(M30-N30)/4	
31	8/2/2024	Control Variable	E	5.82	0.54		Limit Variable	A	AVERAGEIFS(D	AVERAGEIFS(E:E,E	MAXIFS(D:MINIFS(D:MAXIFS(E:MINIFS(E:(K31-L31)/4					(M31-N31)/4	
32	8/2/2024	Control Variable	F	5.4	0.56		Control Variable	C	AVERAGEIFS(D	AVERAGEIFS(E:E,E	MAXIFS(D:MINIFS(D:MAXIFS(E:MINIFS(E:(K32-L32)/4					(M32-N32)/4	
33	8/2/2024	Limit Variable	A	5.49	0.28		Limit Variable	C	AVERAGEIFS(D	AVERAGEIFS(E:E,E	MAXIFS(D:MINIFS(D:MAXIFS(E:MINIFS(E:(K33-L33)/4					(M33-N33)/4	
34	8/2/2024	Limit Variable	C	5.37	0.28		Control Variable	D	AVERAGEIFS(D	AVERAGEIFS(E:E,E	MAXIFS(D:MINIFS(D:MAXIFS(E:MINIFS(E:(K34-L34)/4					(M34-N34)/4	
35	8/2/2024	Limit Variable	D	5.09	0.39		Limit Variable	D	AVERAGEIFS(D	AVERAGEIFS(E:E,E	MAXIFS(D:MINIFS(D:MAXIFS(E:MINIFS(E:(K35-L35)/4					(M35-N35)/4	
36	8/2/2024	Limit Variable	E	5.03	0.35		Control Variable	E	AVERAGEIFS(D	AVERAGEIFS(E:E,E	MAXIFS(D:MINIFS(D:MAXIFS(E:MINIFS(E:(K36-L36)/4					(M36-N36)/4	
37	8/2/2024	Limit Variable	F	5.06	0.39		Limit Variable	E	AVERAGEIFS(D	AVERAGEIFS(E:E,E	MAXIFS(D:MINIFS(D:MAXIFS(E:MINIFS(E:(K37-L37)/4					(M37-N37)/4	
38	8/5/2024	Control Variable	A	5.33	0.56		Control Variable	F	AVERAGEIFS(D	AVERAGEIFS(E:E,E	MAXIFS(D:MINIFS(D:MAXIFS(E:MINIFS(E:(K38-L38)/4					(M38-N38)/4	
39	8/5/2024	Control Variable	C	5.52	0.54		Limit Variable	F	AVERAGEIFS(D	AVERAGEIFS(E:E,E	MAXIFS(D:MINIFS(D:MAXIFS(E:MINIFS(E:(K39-L39)/4					(M39-N39)/4	

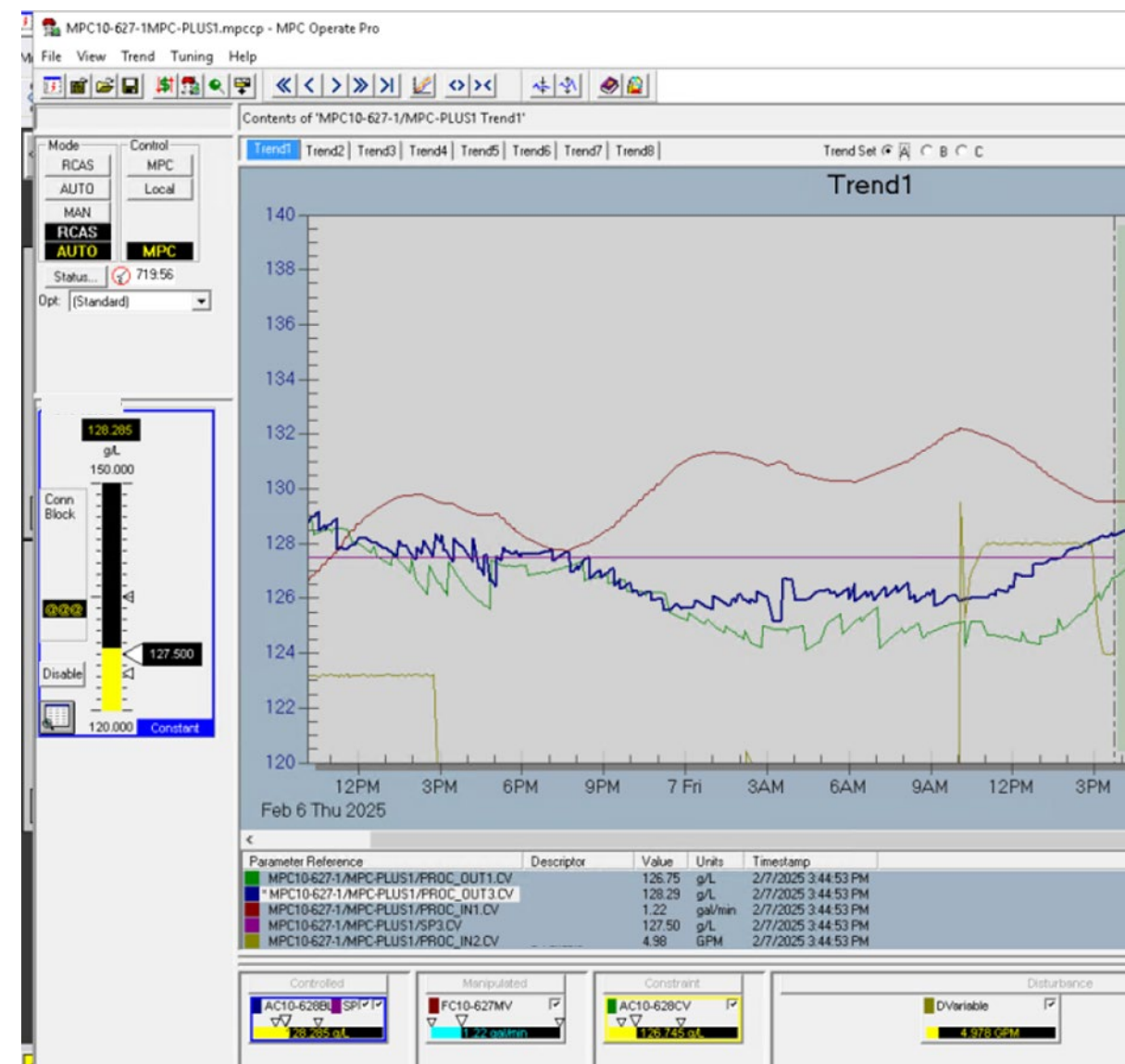
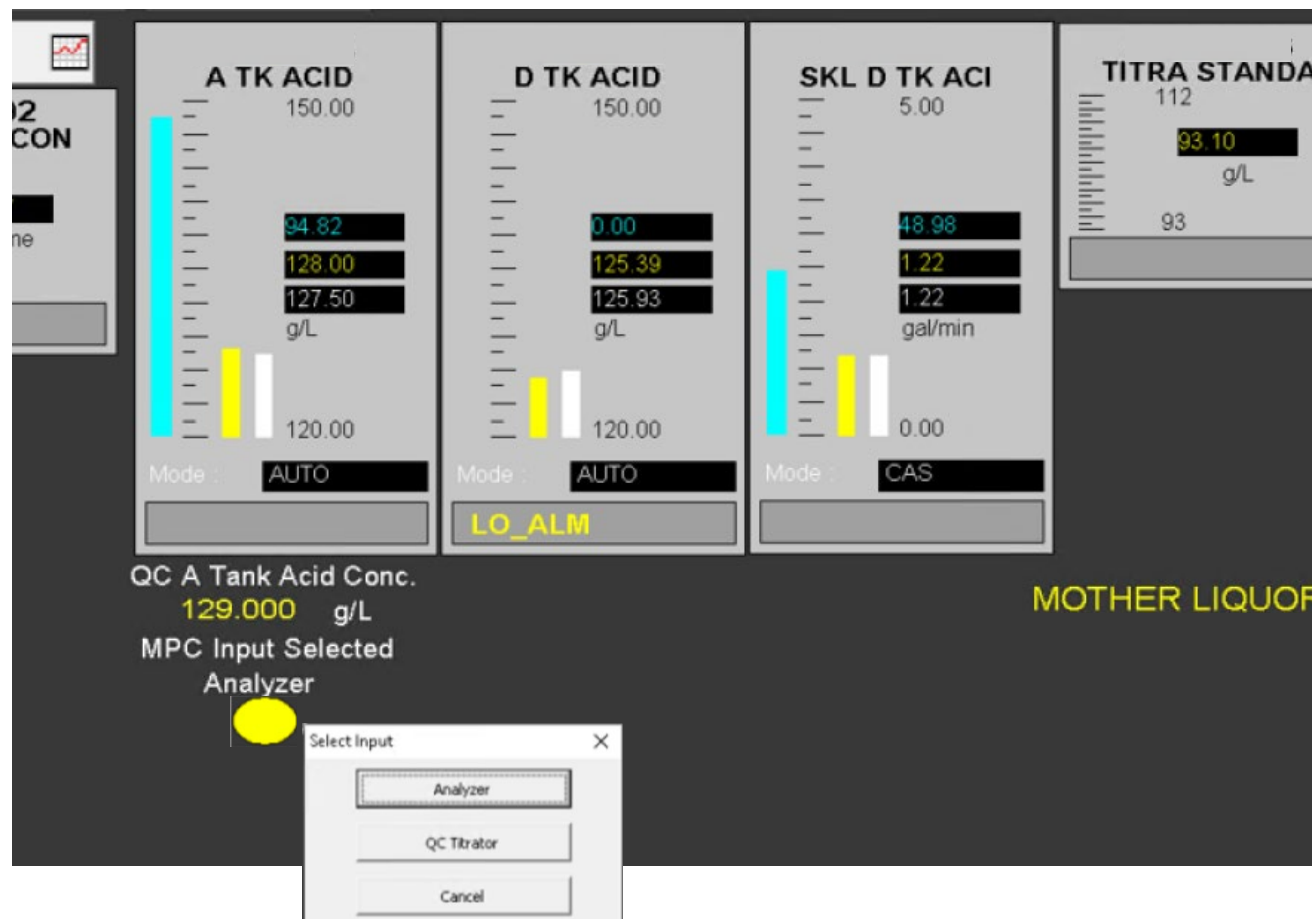
Model Comparison



Model Verification & Editing



Continuous Improvement

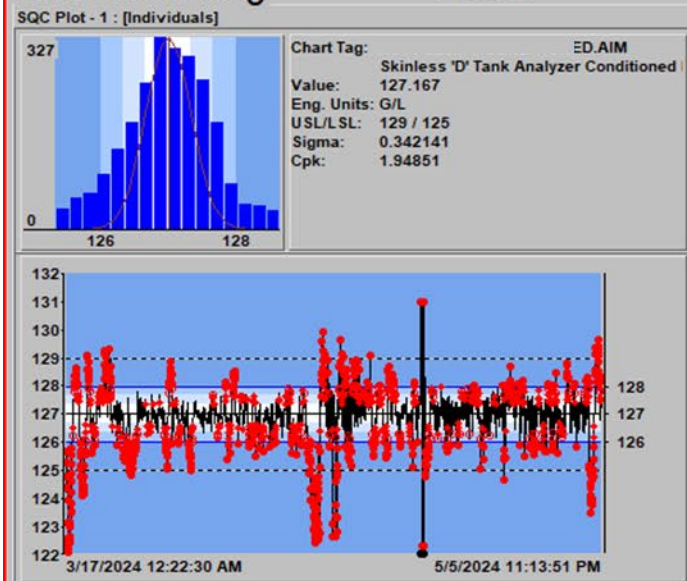


Results

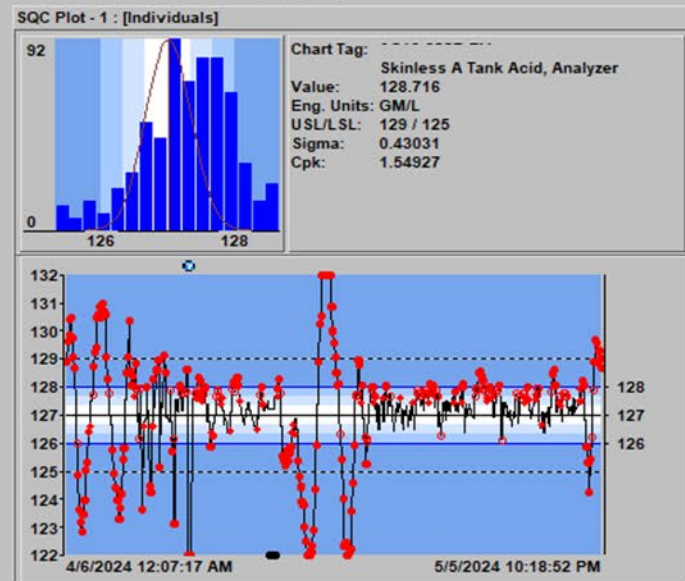
- Even if the AIM control was controlling at acceptable conditions when compared to manual control, it was hard to maintain and was a “black box” for the process engineers; resulting in OPEX and working hours cost.
- MPC achieved a higher CPk than both manual control and control with AIM. PredictPro increases process stability effectively reducing costs.
- Instability in this part of the process can surmount to \$45,000 scrap and waste costs per month in Skinless alone. In Fibrous it can surmount to \$15,000.
- Viscofan can save up to \$60,000 in monthly costs by using the MPC under current production rates.
- Additionally, the control is now democratized and is accessible for a wider audience to maintain, update and scale up.

Results

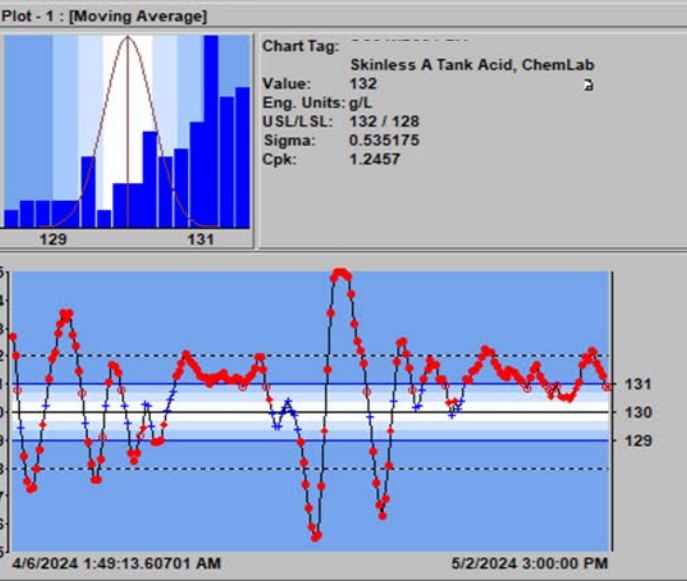
AIM Controlling Dtank



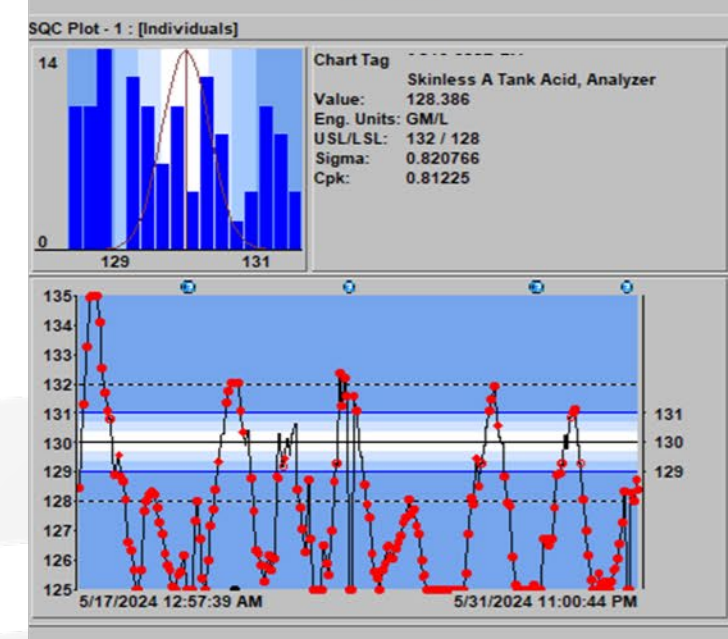
Atank



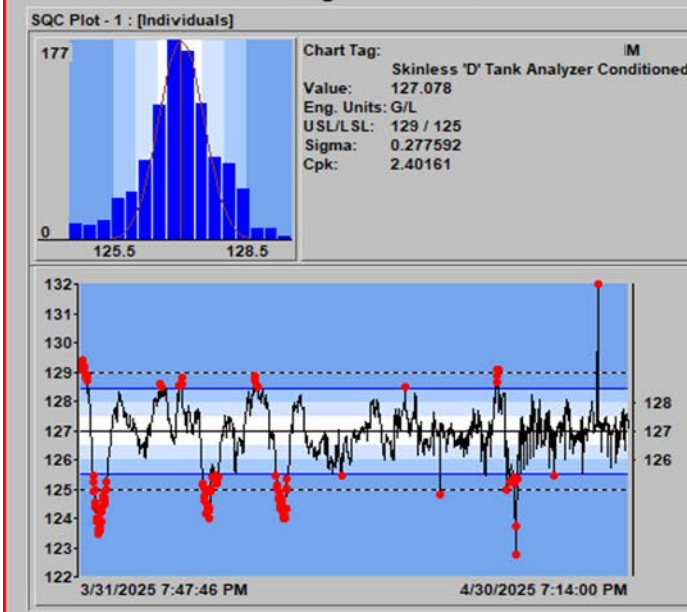
Atank lab test



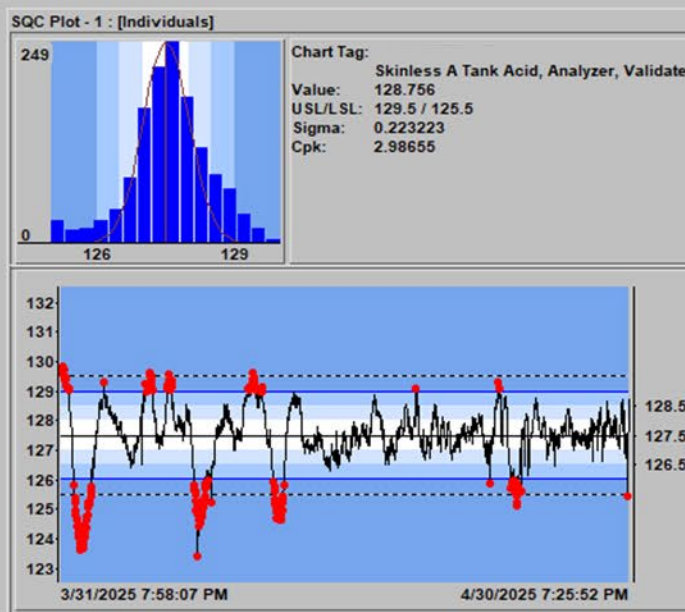
Atank



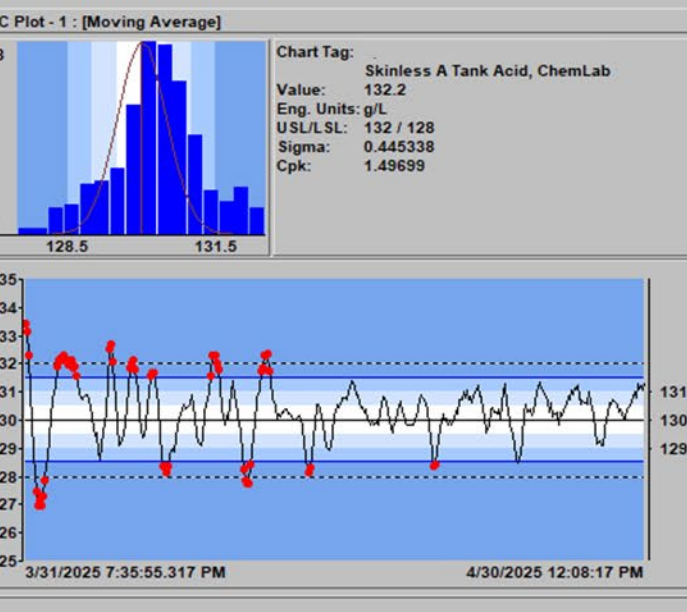
MPC Controlling Dtank



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Atank lab test



Conclusions

It's that Easy

- Marcelo started the project having NO experience with DeltaV, MPC, and obvious lack of experience in the legacy AIM and PROVOX systems.
- The project transformed complex control logic into a graphical and user-friendly interface, removing the need for advanced programming skills.
- The project proved a dynamic and flexible approach like the MPC can have better results than an expert system.
- This project challenged the adage that you can only choose two out of speed, cost-efficiency, and quality—because it successfully delivered all three.



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Questions?

Find More Information

Visit the DeltaV Advanced Control Exhibit

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Thank You